

**Patent claims**

1. A method for treatment of gas exiting the anode side (301) of a solid oxide fuel cell stack (1) fuelled with a carbon containing fuel (100) in a power producing process, characterized in that the anode gas and cathode gas are kept separated by a seal system in the SOFC stack (4) and that the main part of the H<sub>2</sub> and CO in the anode exhaust (351) is separated from the CO<sub>2</sub> in said exhaust (301) by a separation process based on H<sub>2</sub> selective membranes (350).

2. A method according to claim 1, characterized in that the anode exhaust (359) is treated such that most of the CO<sub>2</sub> is not emitted to the atmosphere.

3. A method according to claim 1, characterized in that steam (361) is injected on the permeate side of the hydrogen selective membranes (350).

4. A method according to claim 1, characterized in that the recovered H<sub>2</sub> (355) is fed back to the main SOFC stack (1) and used as fuel.

5. A method according to claim 1, characterized in the recovered H<sub>2</sub> (355) is used to heat the oxygen depleted air (206) entering the expander (207).

6. A method according to claim 1, characterized in that the recovered H<sub>2</sub> (355) is used to heat the air entering the SOFC stack (205).

7. A method according to claim 1, characterized in that the recovered H<sub>2</sub> (355) is exported as a sales product.

8. A method according to claim 1, characterised in that recovered  $H_2$  (355) is fed to the desulphurisation unit (101) to provide necessary hydrogen for hydrodesulphurisation.

5 9. A method for treatment of gas exiting the anode side (301) of a solid oxide fuel cell stack (1) fuelled with a carbon containing fuel (100) in a power producing process, characterised in that the anode gas and cathode gas are kept separated by a seal system in the SOFC stack  
10 (4), that the main part of the  $H_2$  and CO in the anode exhaust (301) is separated from the  $CO_2$  in said exhaust by a separation process based on compressing (312), drying (319) and cooling (321) to a pressure and temperature where most of the  $CO_2$  is in liquid form (322) and subsequently is  
15 separated from the  $H_2$  and CO in a conventional gravity based separation process (323).

10. A method according to claim 9, characterised in that the anode exhaust (301) is treated such that most of the  $CO_2$  is not emitted to the  
20 atmosphere.

11. A method according to claim 9, characterised in that the recovered  $H_2$  and CO (329) is fed back to the main SOFC stack (1) and used as fuel

12. A method according to claim 9, characterised in that the recovered  $H_2$  and CO (329)  
25 is removed in order to avoid build-up of gases which are non-condensable and non-combustible.

13. A method according to claim 9, characterised in that the recovered  $H_2$  and CO (329)  
30 is fed to the desulphurisation unit (101) to provide the necessary hydrogen for hydrodesulphurisation.

**References**

- [1] "A high-efficiency SOFC hybrid power system using the Mercury 50 ATS gas turbine" Wayne L.Lundberg and Stephen E.Veyo, Siemens Westinghouse Power Generation, USA
- 5 [2]  
<http://www.fuelcelltoday.com/FuelCellToday/IndustryInformation/IndustryInformationExternal/IndustryInformationDisplayArticle/0,1168,318,00.html>
- 10 [3] <http://www.ztekcorp.com/projects.htm>
- [4]  
<http://www.netl.doe.gov/scng/projects/hybrid/pubs/hyb40355.pdf>
- [5]  
15 <http://www.netl.doe.gov/scng/projects/hybrid/pubs/hyb40455.pdf>